

Mike Schultz (and Karen Flack)

$$k/\delta < \frac{1}{50}$$

Re large

k^+ large enough for $c_f \neq f(Re)$

$$\delta^+ > 4k$$

Is Townsend's hypothesis OK?

$$Re^* \sim 9 \times 10^5 - 11 \times 10^6$$

(water tunnel)

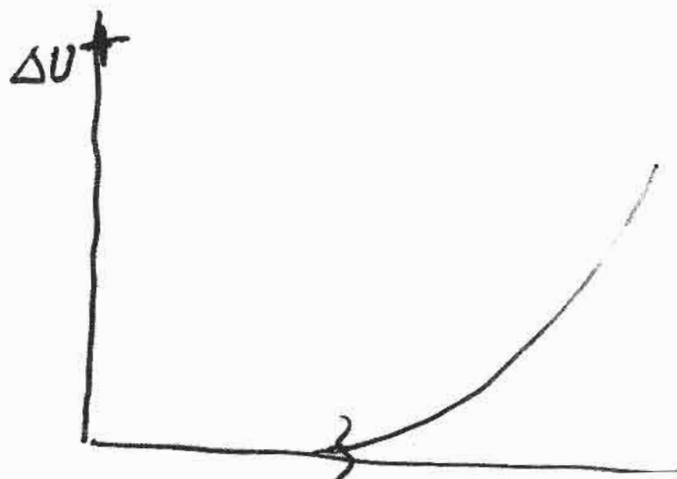
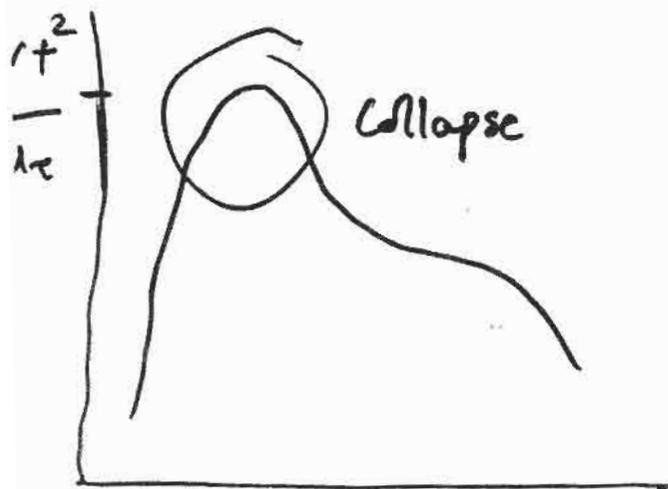
LDV — volume of measurement

(1.3 - 15 in wall units)

$$K_{rms} = 23.6 \mu m$$

$$K_{max}/\delta \sim 10^{-3}$$

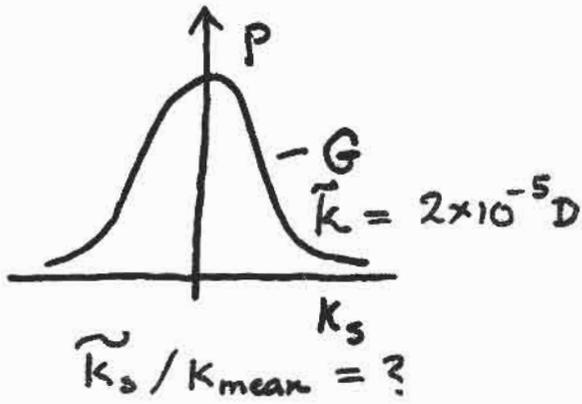
K_y^+ up to 26, δ^+ up to 10k



Smits

Flow in rough pipes

$$(5.7 \times 10^4 < Re < 3.5 \times 10^7)$$

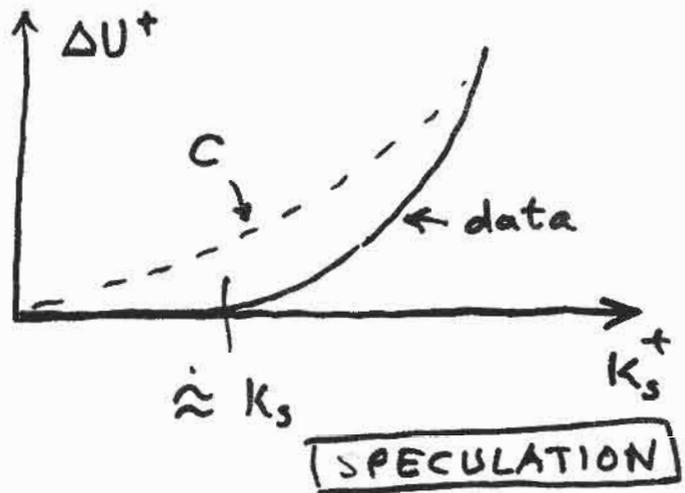


Smooth pipe data of superpipe were indeed smooth for $Re < 2 \times 10^7 \sim 10^7$

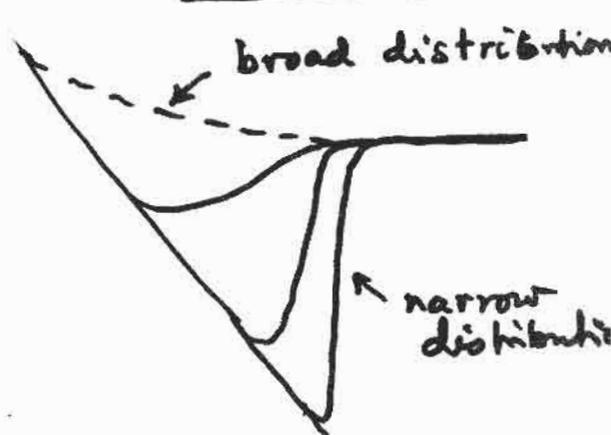
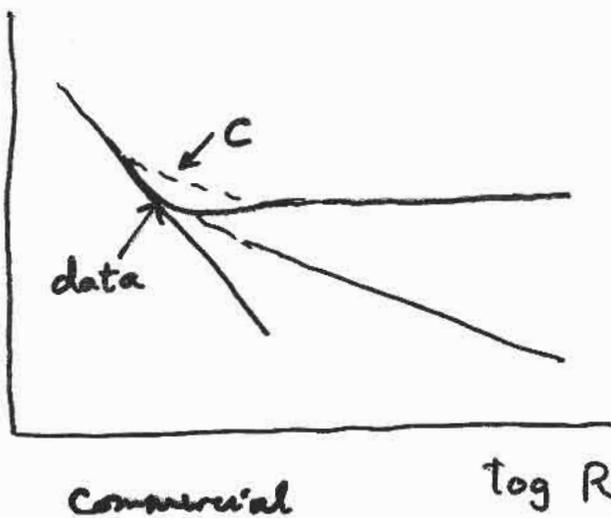
TWO CONCLUSIONS

(1) Colebrook is wrong

Simple Interpolation scheme



(2)
 λ



McKeon

Inertial scaling

$$\delta_v, \eta, \lambda, y, \lambda_s, R$$

$\uparrow\uparrow$
Taylor

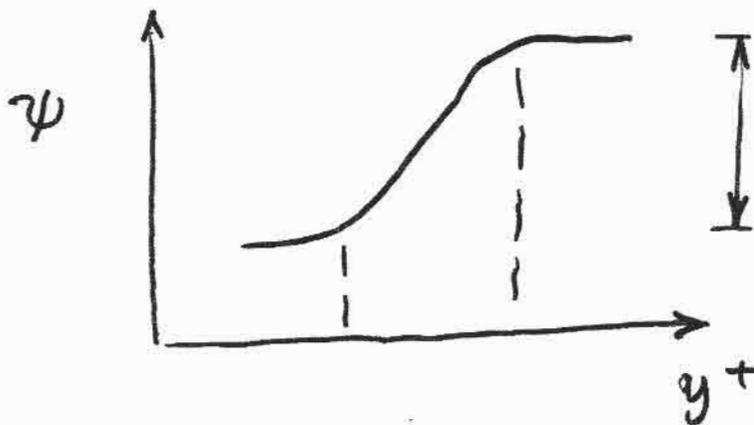
$\uparrow\uparrow$
shear

$$\lambda_s = \sqrt{\frac{\epsilon}{S^3}}$$

$$\lambda > \lambda_s > \eta$$

\vdots

Full similarity needs $Re > 3 \times 10^5$



$$\psi = u^+ - \frac{1}{K} \ln y^+$$

\uparrow
from friction data

"Mixing transition" begins at 7.5×10^4
Full similarity 3×10^5

Mid-Re, high-Re ranges need to be separated!

$$\underline{\lambda_s = \sqrt{\frac{\varepsilon}{S^3}}}$$

In the wall region,

$$\varepsilon = u_\tau^4 / \nu, \quad S = \frac{u_\tau^2}{\nu}$$

$$\lambda_s = \nu / u_\tau$$

$$\eta = \nu / u_\tau$$

In the intermediate region

$$\varepsilon = u_\tau^3 / y$$

$$S = u_\tau / y$$

$$\lambda_s = (\nu / u_\tau)$$

$$\eta = \frac{\nu}{u_\tau} \cdot \left(\frac{y u_\tau}{\nu} \right)^{\frac{1}{4}}$$

In the outer region

$$\lambda_s \approx R, \quad \eta \approx \frac{\nu}{u_\tau} \left(\frac{u_\tau \delta}{\nu} \right)^{\frac{1}{4}}$$

Morrison

large eddies are weak

(Townsend 1956, 1976)

Self-similarity

$$600 < y^+ < 0.12 R^+$$

2nd order str. fn. and spectra

used to deduce influence

of outer scales on the inner

Outer influence — weak

Kunkel

Two aspects:

(1) Nanohotwire

20 nm X 20 nm X 2 μ m

— Have yet to make it work, main remaining task is to lift the sensing element off the large substrate — but progress has been steady.

— Issues of the "free stream" flow ^{in High Pr facility} have been reexamined, work has been done to fix them

Issues of resolution

At some Re

$$l^+ \approx 76, \quad l/\eta \approx 30$$

?

Perhaps OK, perhaps not —

but would be worth repeating

(either in the same flow with better interaction resolution, or a different facility with better resolution)

Turbulent flow in ducts & pipes (MONTY)

$Re_{max} \approx 180 K$ for both

similarity in pipe flow
for $50D$

Not true for ducts!

Remarks for skewness
(not ^{collapsing} overlapping)

u' collapses

Casimir van Doorne

& Frans Nieuwstadt

Turbulence measurements in pipes
using high speed PIV

TRANSITION



travelling waves

Self-sustaining vs transient growth

7 talks

Talamelli

CICLOPE

$$Re_D = 2 \times 10^6, U_{CL} = 50 \text{ m/s}$$

$$D = 0.9 \text{ m}, L = 10^2 \text{ m}$$

|
130 m

Roughness $\sim 10 \mu\text{m}$

Manusic

Construction to begin
Spring 06

Report on the previous meeting
at the CICLOPE site

Total cost $\sim 4 \text{ M€}$
(50% instrumentation)

600K from Bologna
250K from Stockholm
Region, EU

Synchrotron sources, CERN
international facilities