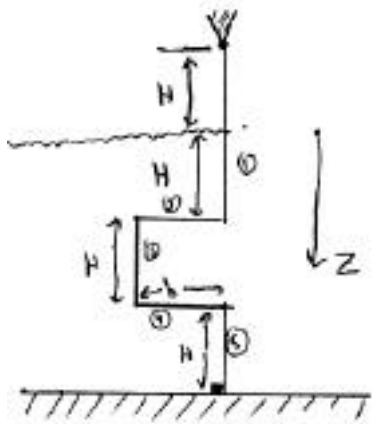


Homework #3 - Solutions

2.43 A rigid gate of width w is hinged without friction at a point H above the surface. Find the ratio b/H at which the gate is about to open



- Assume:
- 1) weight of gate is negligible
 - 2) negligible friction in hinge
 - 3) $\rho = \text{constant}$ (incompressible)
 - 4) $g = \text{constant}$
 - 5) $P_{\text{above water}} = P_{\text{to right of gate}} = P_a$

Gate opens when the moment about the hinge becomes positive (ie counterclockwise) so the critical point is when $\sum \text{moments} = 0$

$\tilde{M}_0 = \tilde{S} \times \tilde{F}$ or $M_0 = \int_0^{2H} \rho g (H+z) z dz$ (vertical piece)
 $F = \text{hydrostatic pressure} = \rho g z$
 $s = 1$ distance from hinge) $M_0 = \int_0^b \rho g (s-z) s ds$ (horizontal piece)
 $= \frac{\rho g}{2} (\cdot z) b^2$

section ①: $\rho g \left(\frac{H^2}{2} - \frac{z^3}{3} \right)_0^H = \left[\frac{1}{2} H^3 - \frac{1}{3} H^3 \right] \rho g$

section ②: $\rho g \left(\frac{H^2}{2} - \frac{z^3}{3} \right)_H^{2H} = \left[2H^3 - \frac{8}{3} H^3 - \left(\frac{1}{2} H^3 - \frac{1}{3} H^3 \right) \right] \rho g$

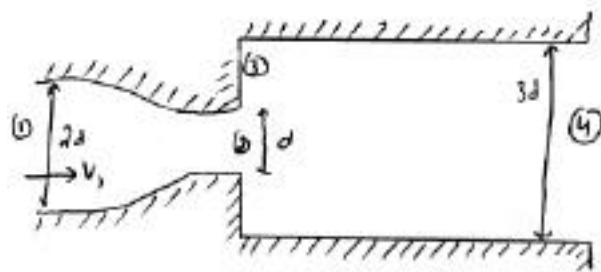
section ③: $\rho g \left(\frac{H^2}{2} - \frac{z^3}{3} \right)_{2H}^{3H} = \left[\frac{9}{2} H^3 - 9H^3 - \left(2H^3 - \frac{8}{3} H^3 \right) \right] \rho g$

section ④ $\frac{\rho g}{2} (2H) b^2 = \frac{1}{2} \rho g b^2 H$

section ⑤ $-\frac{\rho g}{2} (2H) b^2 = -\rho g b^2 H$ (add)

$\rho g \frac{27}{2} H^3 - \frac{1}{2} \rho g b^2 H = 0 \Rightarrow 27H^2 = b^2$ or $\boxed{\frac{b}{H} = \sqrt{27} = 5.2}$

- 4.6 For the given duct, pressure at the exit is atmospheric, $p = \text{const}$, duct has constant width w . a) Sketch flow pattern b) Can Bernoulli's equation be used from 2 \rightarrow 4? c) Is $P_2 = P_3$? d) Find P_{2g} in terms of p and V_1 . e) Find P_{1g} in terms of p and V_1 .

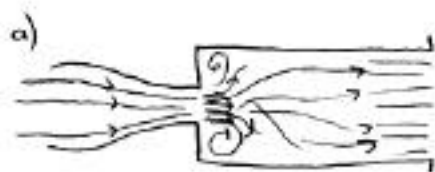


P_a

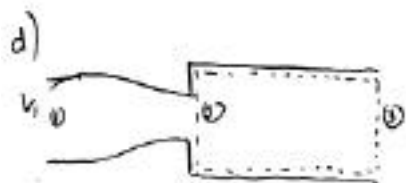
Assumptions:

- 1) $p = \text{const}$
- 2) viscous force on fluid \ll pressure force
- 3) flow is steady (in the mean)
- 4) Uniform (1D) velocity profiles at 1, 2, 4
- 5) $P_4 = P_a$
- 6)

b) No, Bernoulli's can't be used from 2 \rightarrow 4 because the turbulence in the large chamber means there are viscous losses in the flow and streamlines don't exist from 2 \rightarrow 4



c) If P_3 was significantly different from P_2 , the streamlines at 2 wouldn't be parallel to each other; they would be "bent" by the pressure difference so it would be eliminated.



Continuity: $\dot{m} = \text{const} \Rightarrow \dot{m}_1 = \dot{m}_2 = \dot{m}_3$

$$\rho V_1 A_1 = \rho V_2 A_2 = \rho V_3 A_3$$

$$\rho w 2a V_1 = \rho w a V_2 = \rho w 3a V_3$$

$$\Rightarrow V_2 = 2V_1, V_3 = \frac{2}{3}V_1$$

Momentum: $\Sigma F = \text{net outflow of momentum}$

$$P_2 A_2 - P_3 A_3 = -\dot{m} V_2 + \dot{m} V_3$$

$$P_{2g} \cdot 3a = \rho V_1 2a \left(\frac{2}{3} V_1 - 2V_1 \right) \Rightarrow \boxed{P_{2g} = -\frac{8}{9} \rho V_1^2}$$

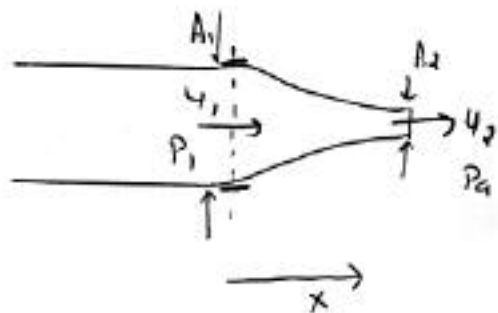
e) use Bernoulli from 1 to 2

$$\frac{P_1}{\rho} + \frac{1}{2} V_1^2 = \frac{P_2}{\rho} + \frac{1}{2} V_2^2 = \frac{P_a}{\rho} - \frac{8}{9} \rho V_1^2 + \frac{1}{2} V_2^2$$

$$P_{1g} = \rho \left[\frac{1}{2} V_2^2 - \frac{8}{9} V_1^2 - \frac{1}{2} V_1^2 \right] = \rho \left[2V_1^2 - \frac{8}{9} V_1^2 - \frac{1}{2} V_1^2 \right] \Rightarrow$$

$$\boxed{P_{1g} = \frac{11}{18} \rho V_1^2}$$

- 4.12 Incompressible, 1D flow exits steadily into the ambient atmosphere from the contraction which is bolted onto a constant area duct. Area ratio $A_1/A_2 = 4$. If the total force on the bolts is F_x , find $F_x/\rho u_1^2 A_1$. Would the analysis hold if flow direction was reversed?



- Assume: 1) $p = \text{const}$
 2) steady
 3) 1-D flow
 4) viscous forces can be neglected
 5) $P_2 = P_a$

From momentum equation:

$$\sum F = \text{net outflow of momentum}$$

in x-direction:

$$-F_x + P_1 A_1 - P_2 A_1 = -\rho A_1 u_1^2 + \rho A_2 u_2^2$$

From continuity:

$$\dot{m} = \text{const} = \rho u_1 A_1 = \rho u_2 A_2 \Rightarrow u_2 = u_1 \frac{A_1}{A_2} = 4u_1$$

From Bernoulli (all 4 conditions ok)

$$\frac{P_1}{\rho} + \frac{1}{2} u_1^2 = \frac{P_2}{\rho} + \frac{1}{2} u_2^2 = \frac{P_2}{\rho} + \frac{1}{2} (4u_1)^2$$

$$P_2 = P_a \quad P_1 = P_a + \frac{15}{2} \rho u_1^2$$

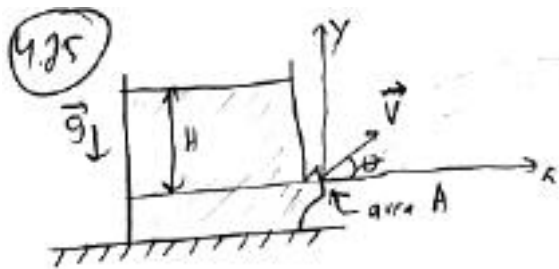
$$\therefore -F_x + [P_a + \frac{15}{2} \rho u_1^2 - P_a] A_1 = \rho A_1 [-u_1^2 + \frac{A_2}{A_1} u_2^2] = \rho A_1 [\frac{1}{4} (4u_1)^2 - u_1^2]$$

$$-F_x = -\frac{15}{2} \rho u_1^2 A_1 + 3 \rho u_1^2 A_1$$

$$\boxed{\frac{F_x}{\rho u_1^2 A_1} = \frac{9}{2}}$$

If flow is reversed P_2 must be $< P_a$.
 (to 'suck' air into the duct). In this case, the streamlines are different at 2 due to the unequal pressures at that point \Rightarrow new problem.





Jet issues smoothly from hole.
 Find max jet height (depending on H and θ).
 Find horizontal force exerted on tank.
 Ignore losses

- Assumptions:
- 1) no losses (no viscosity)
 - 2) tank is so big that H is constant (quasi-steady)
 - 3) $P_{jet} = P_{atm}$
 - 4) 1D flow in jet
 - 5) ~~height~~ width of jet is small (ie neglect height differences in vertical jet cross-section)

Apply Bernoulli from surface to jet exit:

$$\frac{P_{atm}}{\rho} + \frac{1}{2} V_s^2 + gH = \frac{P_{atm}}{\rho} + \frac{1}{2} V_j^2 + g(\theta)$$

$$\text{or } \frac{1}{2} V_j^2 = gH \Rightarrow V_j = \sqrt{2gH}$$

Apply Bernoulli from jet exit to max jet height:

$$\frac{P_{atm}}{\rho} + \frac{1}{2} V_j^2 + g(\theta) = \frac{P_{atm}}{\rho} + \frac{1}{2} V_{max}^2 + gh_{max}$$

V has 2 components: $V_x = V \cos \theta$ $V_y = V \sin \theta$ ($V_y = 0$ at max height)
($V_x = \text{constant in jet}$)

$$\frac{1}{2} V_{jx}^2 + \frac{1}{2} V_{jy}^2 = \frac{1}{2} V_{ix}^2 + \frac{1}{2} (0) + gh_{max}$$

$$\uparrow = \frac{1}{2} (V_{hmax})^2 \quad \Rightarrow \quad h_{max} = \frac{1}{2g} V_{jy}^2 = \boxed{H \sin^2 \theta = h_{max}}$$

Use x-mom eqn:

$\sum F_x = \text{net x-mom. outflow}$

$$\sum F_x = \int p V_x (\vec{v} \cdot \vec{n}) dA \quad \leftarrow \text{notice I drew CV so } \vec{n} \cdot \vec{v} = V_j$$

$$\sum F_x = \rho V_x V_j A = \rho V_j^2 \cos \theta A$$

$$\sum F_x = R_x \quad (\text{pressure is equal at both left and right boundaries})$$

(R_x is force required to hold tank in place - by friction at lower surface maybe)

$$\boxed{R_x = \rho V_j^2 \cos \theta A} \quad = \quad \boxed{2\rho g H A \cos \theta}$$

